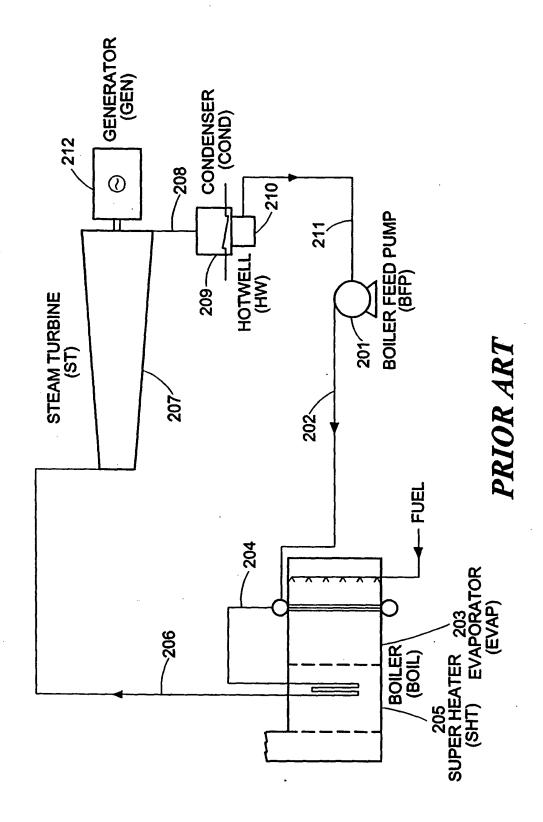


FIG. 2



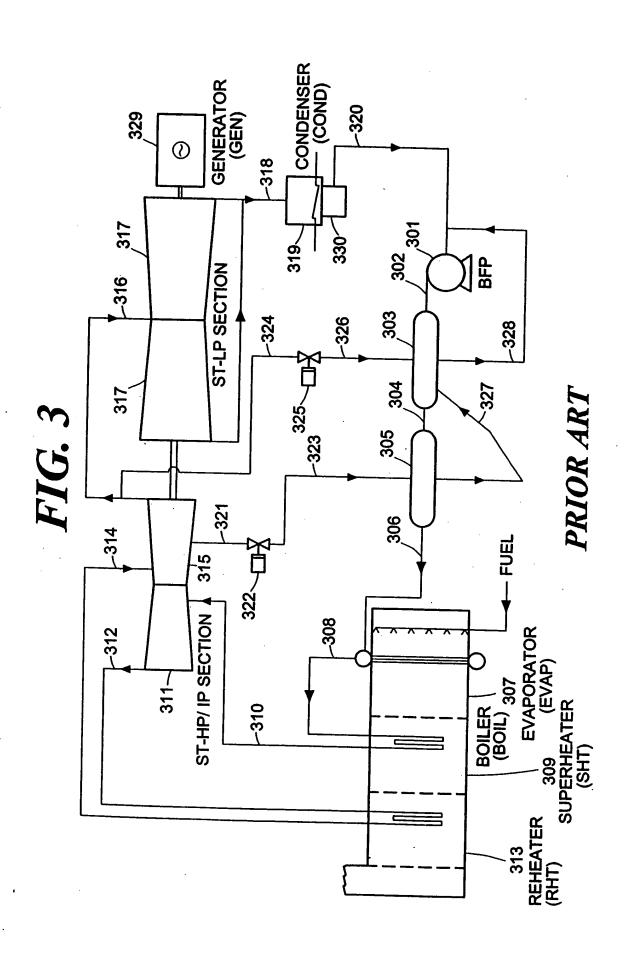
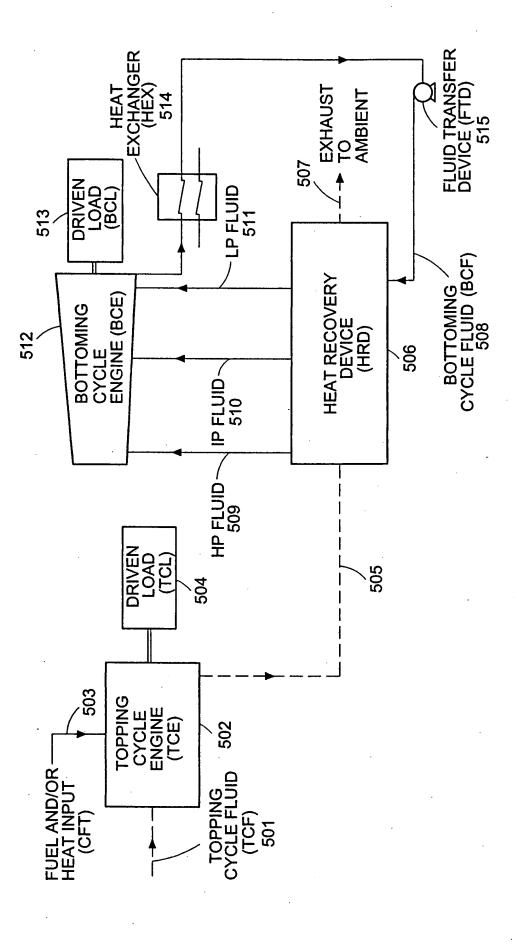


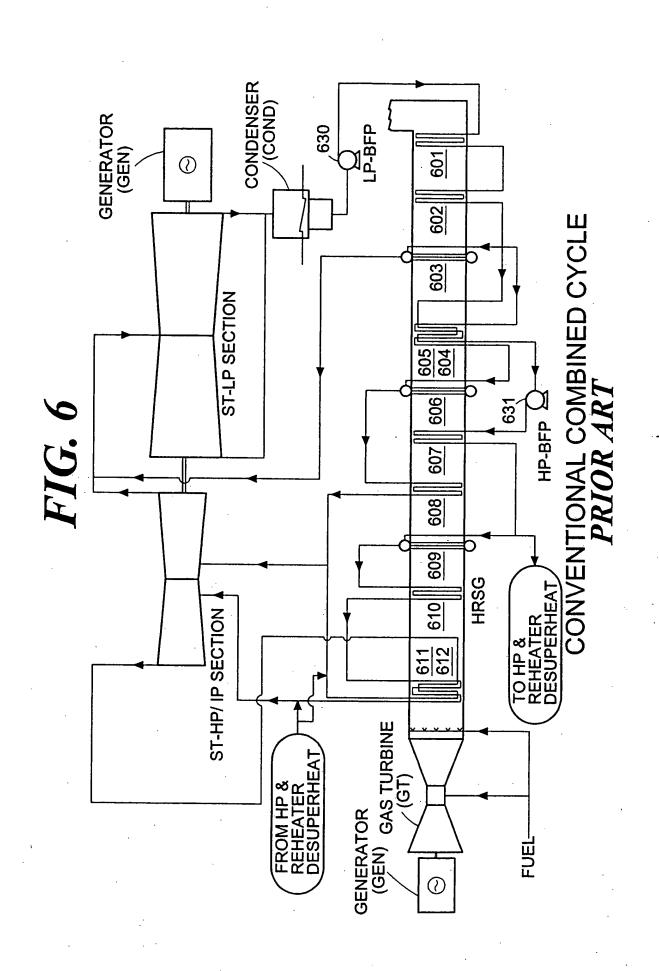
FIG. 4

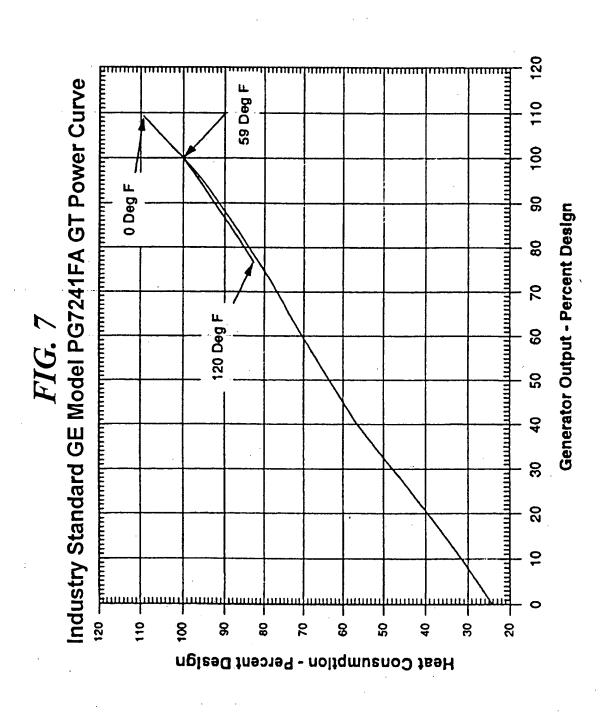
Rankine Cycle Comparison

		_							
Efficiency Improvement	%		Base	%6 <i>L</i> ′4	%59'9	8.93%	10.35%	13.30%	16.28%
Efficiency	%		40.23%	42.15%	42.90%	43.82%	44.39%	45.58%	46.78%
Input	BTU/ Ibm		1458.5	1642.4	1633.9	1257.1	1214.3	1866.0	1564.4
Output	BTU/ Ibm		286.7	692.3	701.0	550.9	539.1	850.5	731.8
Second Extract Flow	%		N/A	N/A	N/A	8.11	7.95	W/A	14.12
First Extract Flow	%		N/A	N/A	N/A	21.76	24.81	N/A	8.72
Exhaust Pressure	psia		0.5894	0.5894	0.5894	0.5894	0.5894	0.5894	0.5894
Reheat Temp	Degrees F		N/A	1050	1050	1050	1050	1112	1112
Reheat Press	psia		YN.	480.0	640.0	480.0	640.0	1029.0	1029.0
Inlet Temp Reheat Press	Degrees F		1050	1050	1050	1050	1050	1070	1070
Inlet Press	psia		1800	1800	2400	1800	2400	3860	3860
Description			Simple, No Reheat, No FWH	Reheat, No FWH	Reheat, No FWH, Higher Press	Reheat, With FWH	Reheat, With FWH, Higher Pressure	Supercritical, Double Reheat, No FWH	Supercritical, Double Reheat, With FWH
Option			-	2	က	4	ις .	ဖ	7

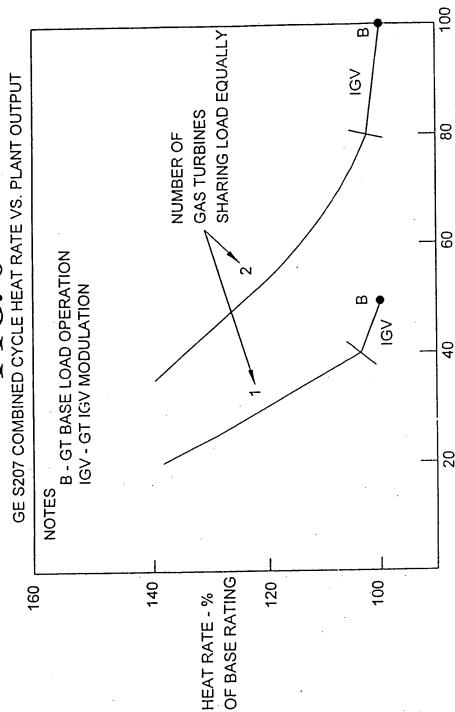
FIG. 5











FLANT OUTPUT - % OF BASE RATING

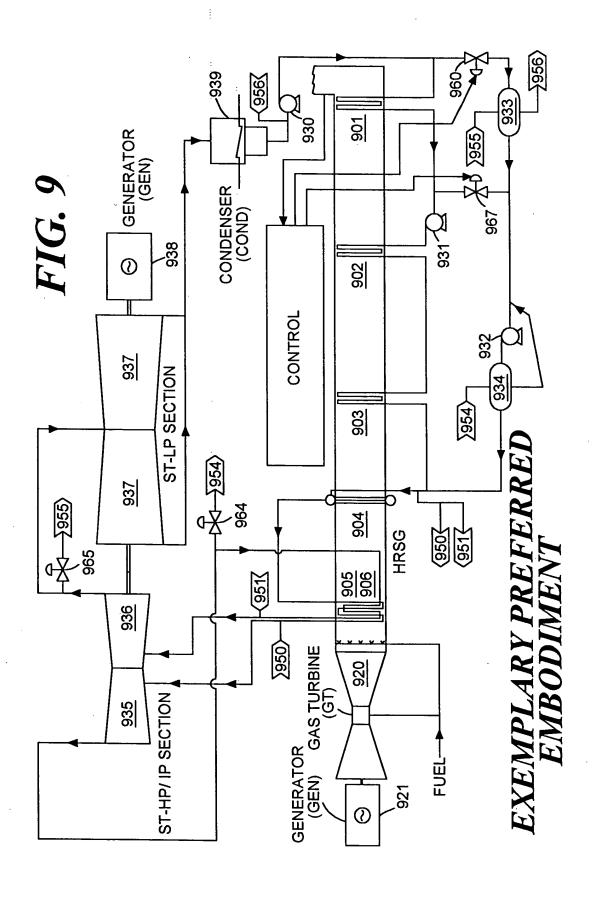
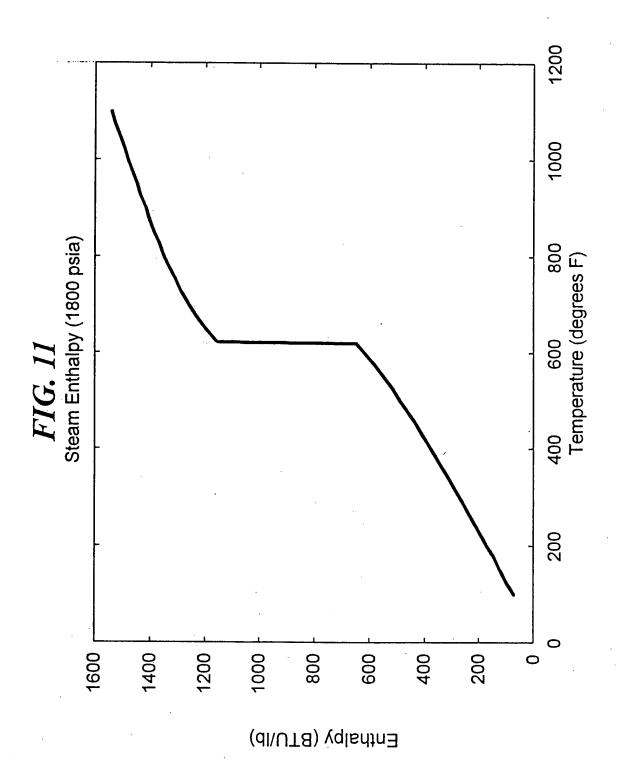


FIG. 10

Energy Flow Analysis Comparison

HR-LHV	(PHR)	BTU/kW		6041	5942
Plant Eff	(CCE)		20.90%	20.90%	51.75%
Aux STG Eff ST Out Plant Eff HR-LHV	(STO)	% of GTI	18.59%	34.76%	91.72% 46.78% 97.50% 99.00% 41.42% 51.75%
STG Eff	(AXF) (1-SGL)	%	%00'66	81.13% 44.39% 97.50% 99.00%	%00'66
Aux	(AXF)	Factor	97.50%	97.50%	97.50%
SC Eff	(SCE)	%	38.78%	44.39%	46.78%
HRSG Stm	(HGS)	% of GTI			
HRSGL	(HGL)		0.50%	0.82%	0.93%
Exh Loss	(HGE)	% of GTI % of GTI	6.04%	6.04%	6.04%
Option GT Output GT Loss Supp Fire HRSG Input Exh Loss	(HGI)	% of GTI	56.21%	87.99%	%69'86
Supp Fire	(SFE)	% of GTI	32.31% 11.48% 0.00%	32.31% 11.48% 31.78%	42.48%
GT Loss	(GTL) (SFE)	% of GTI	11.48%	11.48%	11.48%
GT Output	(GTO)	% of GTI % of GTI % of GTI	32.31%	l	32.31% 11.48% 42.48%
Option			Prior Art	Example	SuperCrit

Symbol	Description
GTI	GT Input Energy
GTO	GT Generator Electrical Output.
GTL	GT Losses for heat, auxiliaries, generator efficiency
SFE	Energy added through supplemental firing
HGI	GT exhaust energy at inlet to HRSG
HGE	Energy exhausted to atmosphere at HRSG outlet
HGL	HRSG heat loss to ambient
HGS	Energy in HRSG transferred to steam
SCE	Steam cycle basic efficiency
AXF	Factor to account for auxiliary loads in steam cycle
SGL	Steam Turbine generator losses
STO	Steam turbine generator electrical output
CCE	Combined Cycle plant efficiency
PHR	Overall plant heat rate base on LHV of natural gas



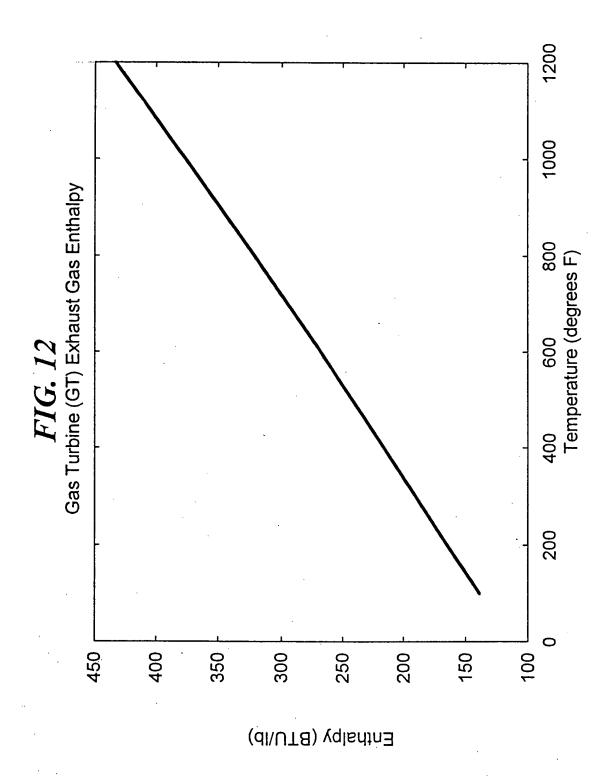
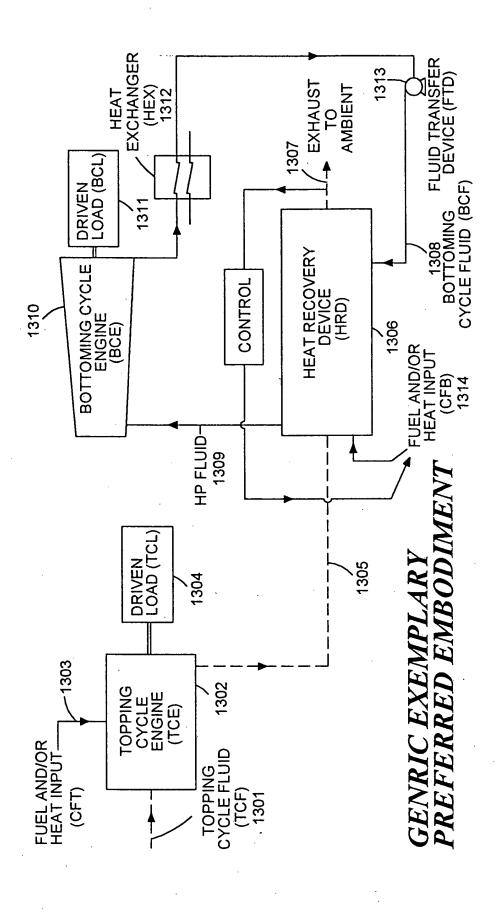
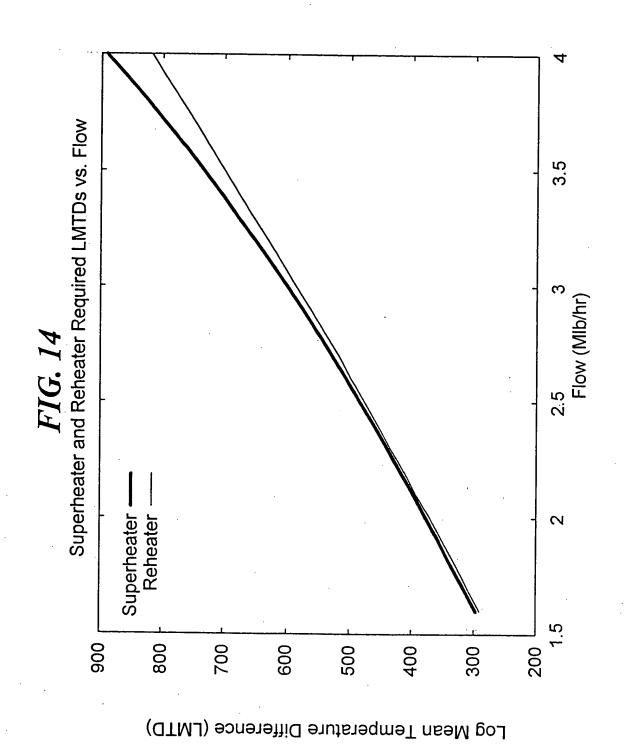


FIG. 13





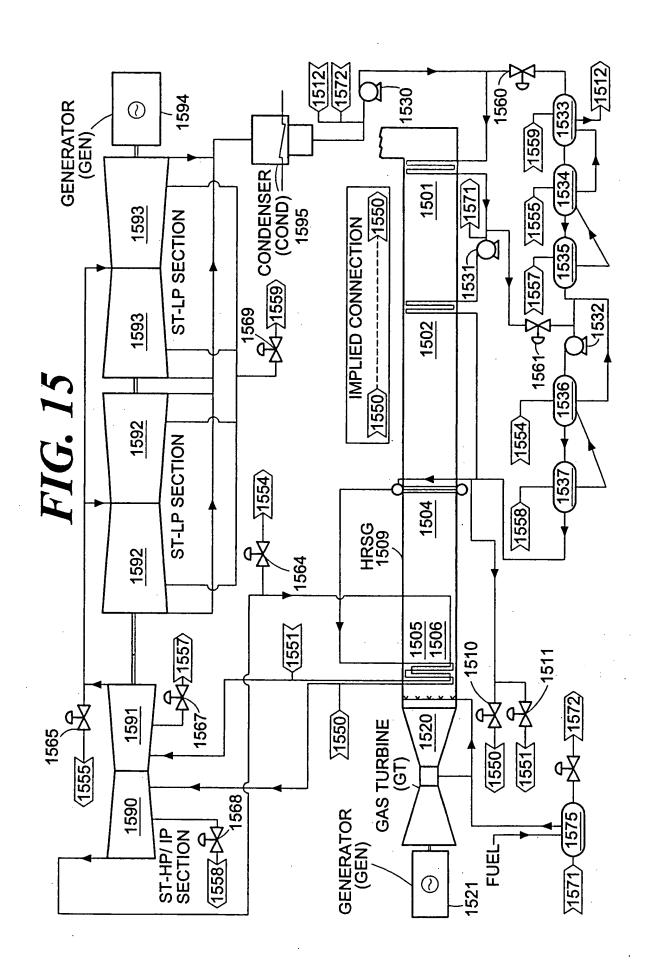
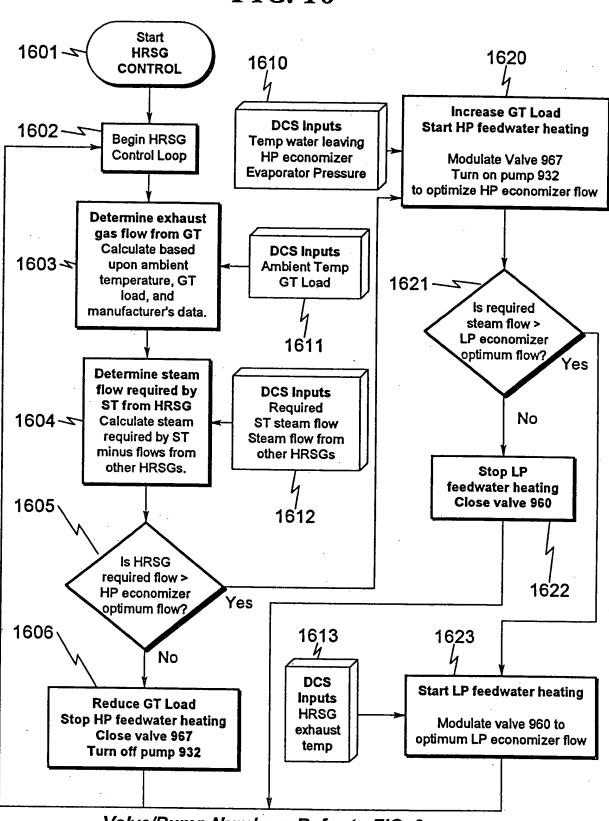


FIG. 16



Valve/Pump Numbers Refer to FIG. 9

FIG. 17

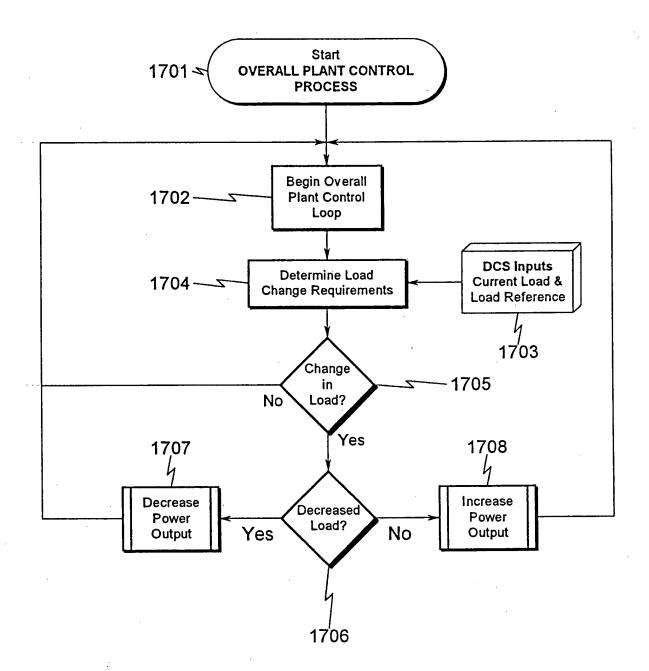


FIG. 18

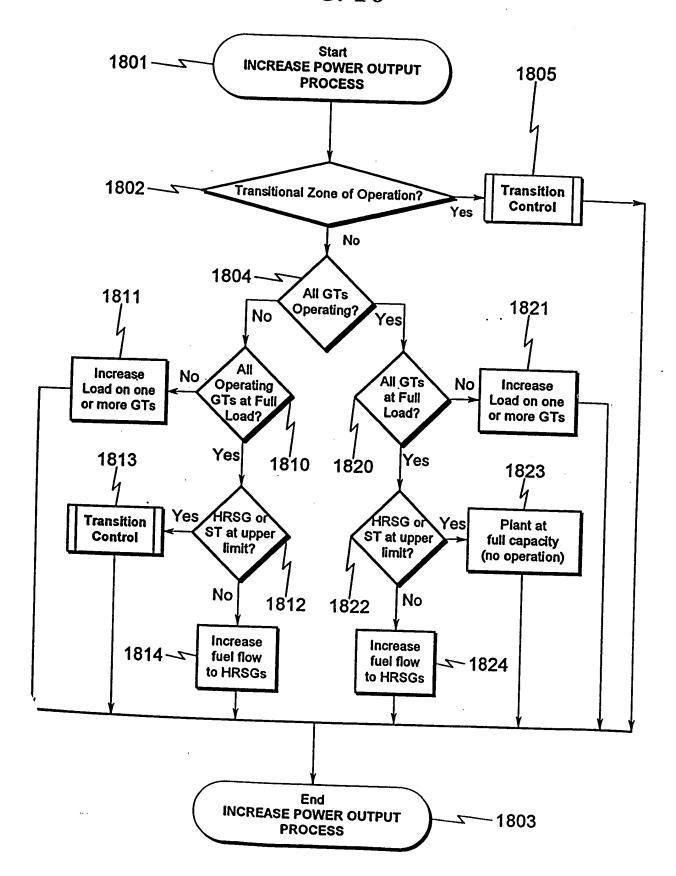


FIG. 19

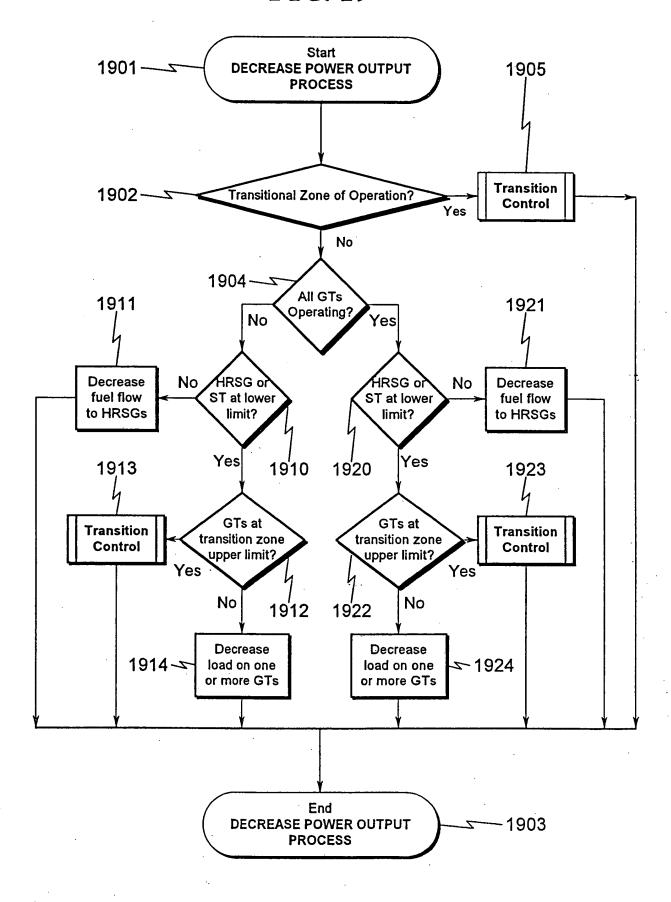
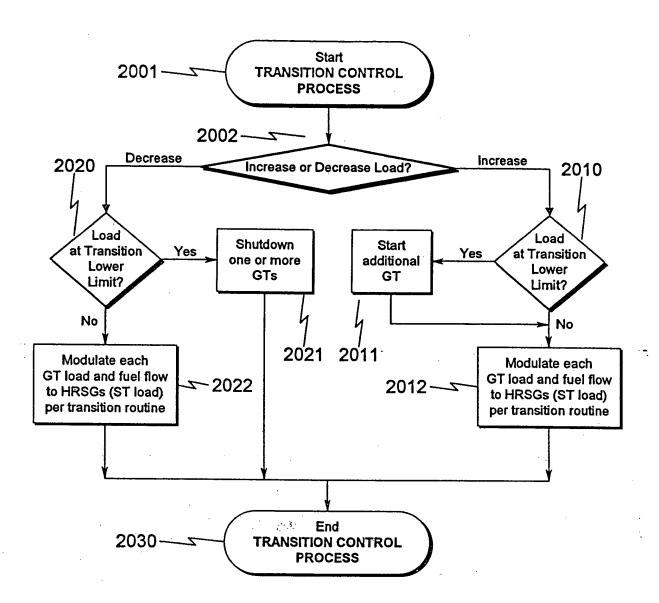
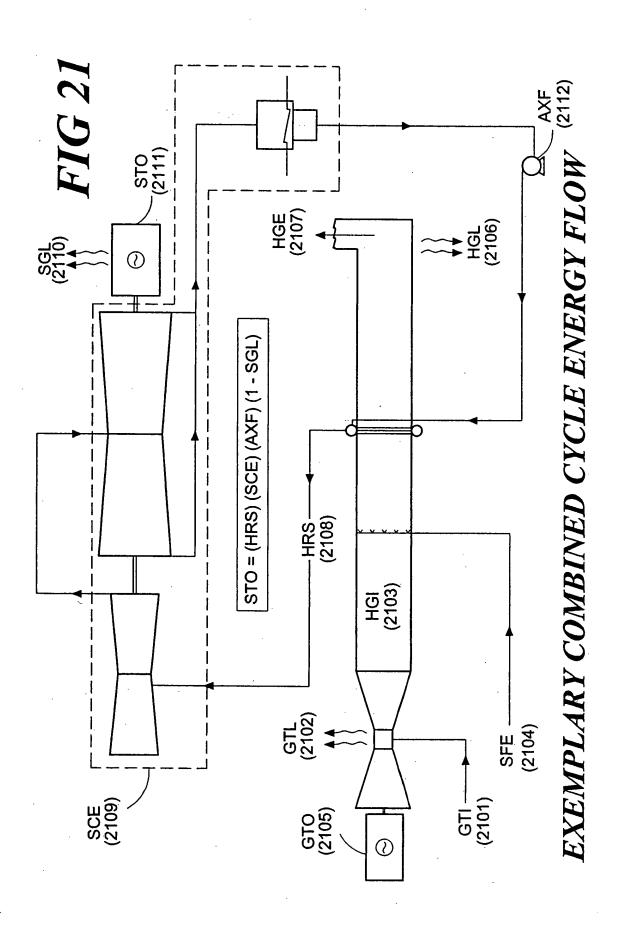


FIG. 20





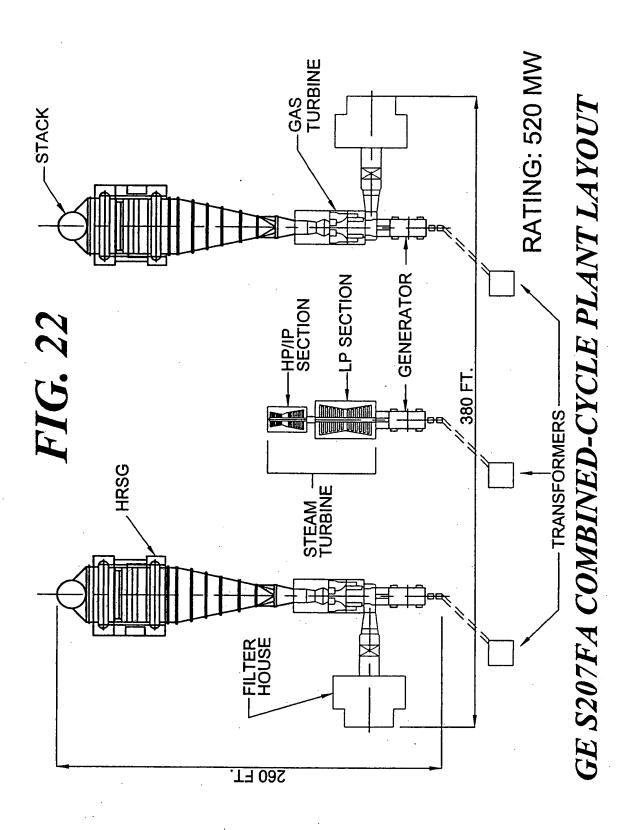


FIG. 23A

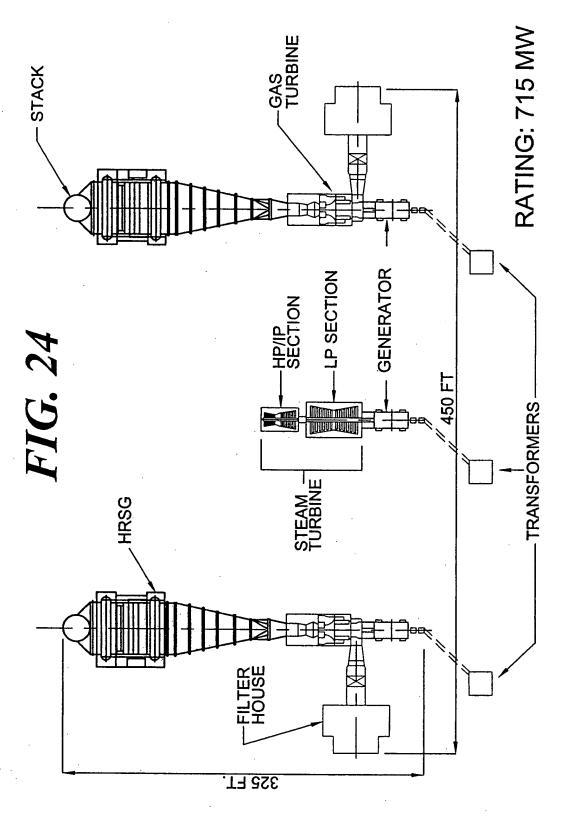
GE S207FA Combined Cycle Power Plant ISO Capacity – 521.6 MW

	Major Equipment					
	Qty Equipment 2 GE Model 7241 FA Gas Turbines	MW	Total MW			
	2 GE Model 7241 FA Gas Turbines	168.8	337.6			
	1 GE 1800 psig steam turbine	190.0	190.0			
	2 HRSGs, three pressure levels					
	1 Auxiliary equipment	-6.0	-6.0			
	(BFPs, circulation pumps, etc.)		*			
	Net Plant Output	<u>521.6</u>	MW			
Ī	Plant Operation Pro	ofile				
_	Hours per Week @ Peak Power	20				
	Peak Power Heat Rate Correction	1.00				
	% of Peak Power	1.00				
	Hours per Week @ Intermediate Power Level	. 71				
	Intermediate Power Heat Rate Correction	1.02				
	% of Peak Power	0.80				
	Hours per Week @ Night Power Level	77				
	Night Power Heat Rate Correction	1.19				
	% of Peak Power	0.60				
	Plant Performance	e	,			
_	Plant heat rate at full load	6040	BTU/kWh			
			LHV			
	Natural gas fuel ratio HHV/LLV	1.11	•			
	Plant Capacity Factor	73.21	%			
	Heat Rate Correction Factor for Off Peak Operation	1.0806				
	Plant Availability	8500	hours/yr			
	Average Natural Gas Cost	\$3.00	per MMBTU			
	Annual Electric Production	3,246,028,571	kWh			
	Annual Fuel Consumption	23,516,781	MMBTU			
	Annual Fuel Cost	<u>\$70,550,343</u>				

FIG. 23B

GE S207FA Combined Cycle Power Plant ISO Capacity – 521.6 MW

Plant Capital Costs					
Average Installed Cost	\$425	\$/kW			
Total Plant Cost	\$221,680,000	•			
Interest Rate	8.00%				
Finance Period	20	years			
Annual Loan Payment (12 monthly installments)	<u>\$22,250,644</u>				
Plant Maintenance					
GT Maintenance Cost	\$0.0025	per kWh			
ST Maintenance Cost	\$0.0005				
Average Maintenance Cost	\$0.0018	per kWh			
Annual Maintenance Cost	<u>\$5,777,143</u>				
Net Costs per kWh	n				
Fuel Cost	\$0.0217				
Capital Cost	\$0.0069				
Maintenance Cost	\$0.0018	•			
Total Fuel, Capital, and Maintenance Costs	<u>\$0.0304</u>				
NOx Emissions					
Peak Power Exhaust Flow per Gas Turbine	3,542,000	lb/hr			
Peak Power NOx Levels	9	ppm			
Peak Power Exhaust Flow	100.00%	•			
Intermediate Power NOx Levels	9	ppm			
Intermediate Power Exhaust Flow	85.00%				
Night Power NOx Levels	9	ppm			
Night Power Exhaust Flow	73.00%				
Expected Emissions (No aftertreatment)	352.41	tons/yr			
Expected Emissions (90% Efficient SCR)	35.24	tons/yr			



WESTINGHOUSE 2X1 501G COMBINED-CYCLE PLANT

FIG. 25A

Westinghouse 2X1 501G Combined Cycle Power Plant ISO Capacity – 715.5 MW

	Major Equipment					
Qty 2	Equipment	MW	Total MW			
2	Westinghouse Model 501G Gas Turbines	239.4	478.8			
1	Westinghouse 1800 psig steam turbine	244.7	244.7			
2	HRSGs, three pressure levels					
1	Auxiliary equipment	-8.0	-8.0			
	(BFPs, circulation pumps, etc.)					
	Net Plant Output	<u>715.5</u>	MW			
	Plant Operation Pro	file				
Hour	s per Week @ Peak Power	20				
Peak	Power Heat Rate Correction	1.00				
% of	Peak Power	1.00				
	s per Week @ Intermediate Power Level	71				
	nediate Power Heat Rate Correction	1.02				
	Peak Power	0.80				
	s per Week @ Night Power Level	77				
	Power Heat Rate Correction	1.19				
% of	Peak Power	0.60				
	Plant Performance	 9				
Plant	heat rate at full load	5830	BTU/kWh			
	•		LHV			
	al gas fuel ratio HHV/LLV	1.11				
	Capacity Factor	73.21	%			
	Rate Correction Factor for Off Peak Operation	1.0806				
	Availability	8500	hours/yr			
	age Natural Gas Cost	\$3.00	per MMBTU			
	al Electric Production	4,452,709,821	kWh			
Annu	al Fuel Consumption	31,137,342	MMBTU			
Annı	ual Fuel Cost	\$93,412,027				

FIG. 25B

Westinghouse 2X1 501G Combined Cycle Power Plant ISO Capacity – 715.5 MW

Plant Capital Costs					
Average Installed Cost	\$475	\$/kW			
Total Plant Cost	\$339,862,500				
Interest Rate	8.00%				
Finance Period	20	years			
Annual Loan Payment (12 monthly installments)	<u>\$34,112,954</u>				
Plant Maintenance					
GT Maintenance Cost	\$0.0045	per kWh			
ST Maintenance Cost	\$0.0005	per kWh			
Average Maintenance Cost	\$0.0031	per kWh			
Annual Maintenance Cost	<u>\$14,013,266</u>				
Net Costs per kWh					
Fuel Cost	\$0.0210				
Capital Cost	\$0.0077				
Maintenance Cost	\$0.0031				
Total Fuel, Capital, and Maintenance Costs	<u>\$0.0318</u>				
NOx Emissions	· · · · · · · · · · · · · · · · · · ·				
Peak Power Exhaust Flow per Gas Turbine	4,365,000	lb/hr			
Peak Power NOx Levels	42	ppm			
Peak Power Exhaust Flow	100.00%				
Intermediate Power NOx Levels	50	ppm			
Intermediate Power Exhaust Flow	85.00%				
Night Power NOx Levels	60	ppm			
Night Power Exhaust Flow	73.00%				
Expected Emissions (No aftertreatment)	2554.81	tons/yr			
Expected Emissions (90% Efficient SCR)	255.48	tons/yr			

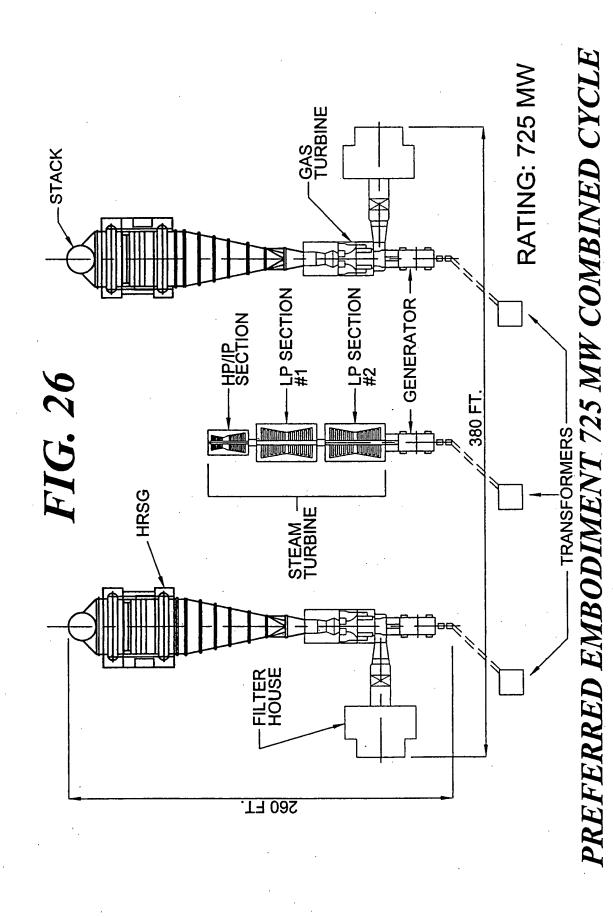


FIG. 27A

Exemplary Preferred Embodiment Combined Cycle Power Plant ISO Capacity – 725 MW

Major Equipment					
Qty Equipment 2 GE Model 7241		MW	Total MW		
	FA Gas Turbines	168.8	337.6		
1 GE 2400 psig st		395.9	395.9		
2 HRSGs, three p					
 Auxiliary equipment 		-8.5	- 8.5		
(BFPs, circulation	•				
	Net Plant Output	<u>725</u>	MW		
	Plant Operation Pro	file			
Hours per Week @ Pea	ak Power	20	·		
Peak Power Heat Rate	Correction	1.00			
% of Peak Power		1.00	•		
Hours per Week @ Inte		71			
Intermediate Power He	at Rate Correction	1.00			
% of Peak Power	0.80				
Hours per Week @ Nig	77				
Night Power Heat Rate	Correction	1.03			
% of Peak Power	0.60				
	Plant Performanc	e			
Plant heat rate at full lo	ad	6006	BTU/kWh		
•			LHV		
Natural gas fuel ratio H	HV/LLV	1.11			
Plant Capacity Factor		73.21	%		
	actor for Off Peak Operation	1.0095			
Plant Availability	· · · · · · · · · · · · · · · · · · ·		hours/yr		
Average Natural Gas Cost		\$3.00	•		
Annual Electric Produ		4,511,830,357			
Annual Fuel Consumpt	ion	30,365,273	MMBTU		
Annual Fuel Cost		<u>\$91,095,818</u>			

FIG. 27B

Exemplary Preferred Embodiment Combined Cycle Power Plant ISO Capacity – 725 MW

Plant Capital Costs					
Average Installed Cost	\$330	\$/kW			
Total Plant Cost	\$239,250,000				
Interest Rate	8.00%				
Finance Period	20	years			
Annual Loan Payment (12 monthly installments)	<u>\$24,014,194</u>				
Plant Maintenance					
GT Maintenance Cost	\$0.0025	per kWh			
ST Maintenance Cost	\$0.0005	per kWh			
Average Maintenance Cost	\$0.0011	per kWh			
Annual Maintenance Cost	<u>\$4,737,422</u>				
Net Costs per kWh					
Fuel Cost	\$0.0202				
Capital Cost	\$0.0053				
Maintenance Cost	\$0.0011				
Total Fuel, Capital, and Maintenance Costs	<u>\$0.0266</u>				
NOx Emissions					
Peak Power Exhaust Flow per Gas Turbine	3,542,000	lb/hr			
Peak Power NOx Levels	20.9	ppm			
Peak Power Exhaust Flow	100.76%				
Intermediate Power NOx Levels	15.29	ppm			
Intermediate Power Exhaust Flow	92.87%				
Night Power NOx Levels	31.26	ppm			
Night Power Exhaust Flow	50.72%				
Expected Emissions (No aftertreatment)	759.90				
Expected Emissions (90% Efficient SCR)	75.99	tons/yr			

FIG 28

Part Load Efficiency Preferred Embodiment vs. Prior Art

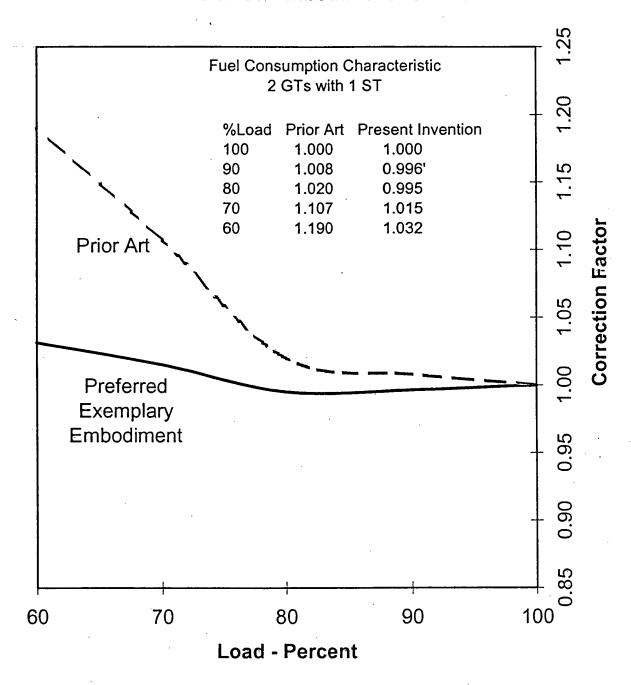
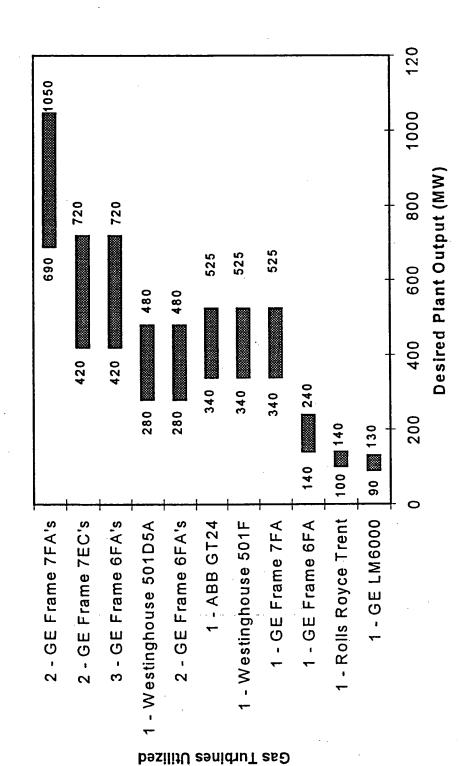
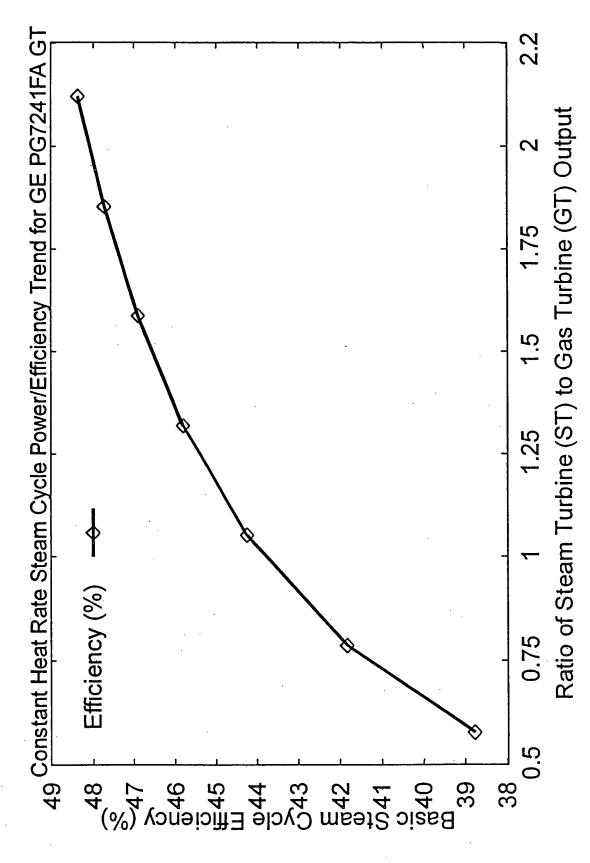


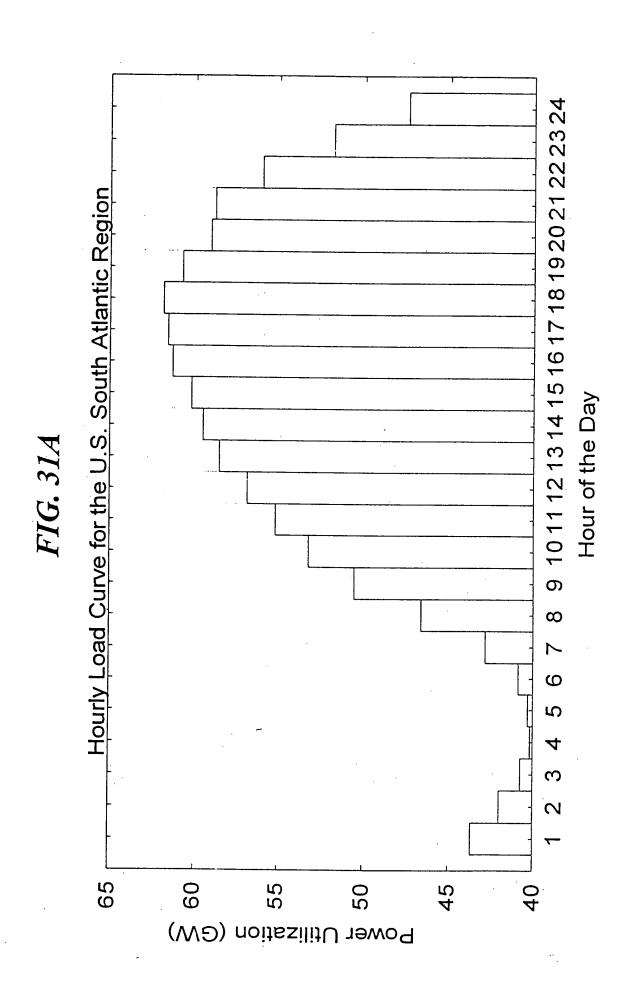
FIG. 29

Preferred Exemplary Embodiment Power Plant Range Selection Chart (Partial Equipment List Using Common Industry Components)









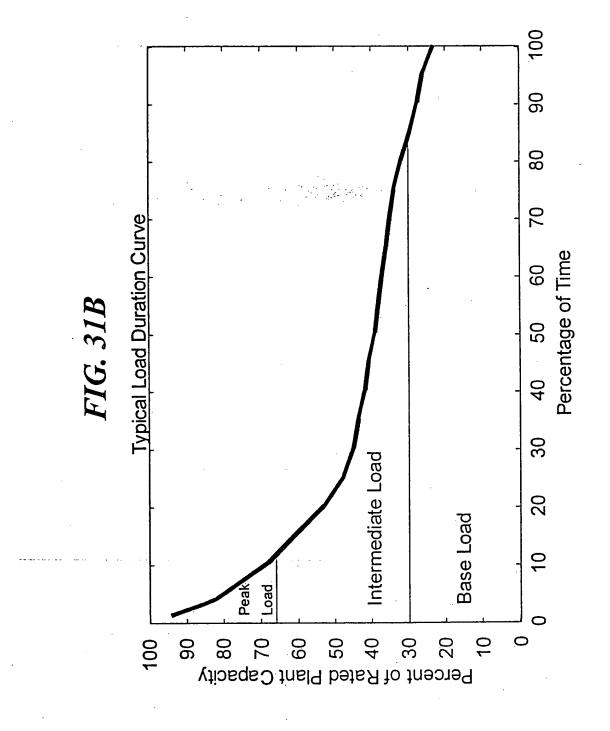


FIG. 32 Typical Load Profile (Based upon DOE Information from FIG. 31A)

System Capacity

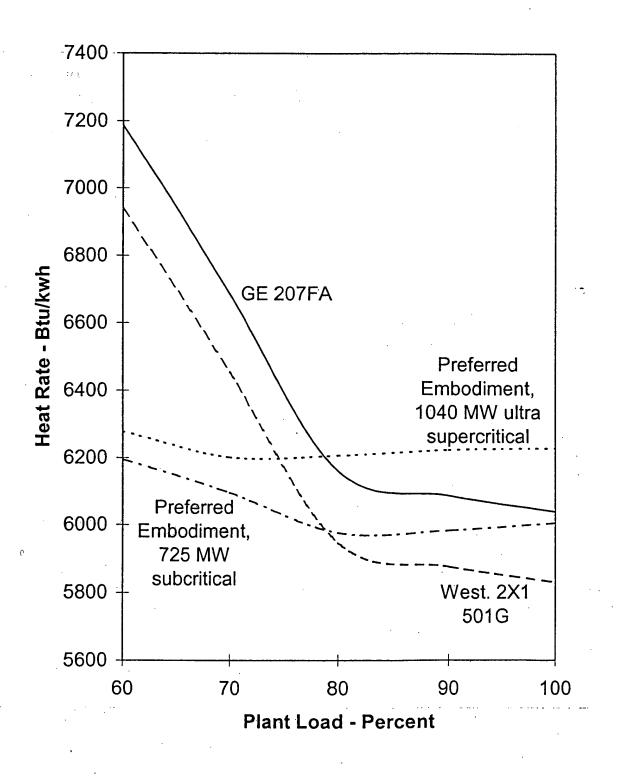
70 GW

Weekday Profile					
Hour	Period	GW			
1	Night	43			
2	Night	42			
3 4	Night	41			
4	Night	40			
5	Night	40			
6	Night	41			
7	Night	42			
8.	Night _	47			
		336			
9	Intermediate	51			
10	Intermediate	53			
11	Intermediate	55			
12	Intermediate	57			
13	Intermediate	59			
14	Intermediate	60			
15	Intermediate _	60			
		395			
16	Peak	61			
17	Peak	62			
18	Peak	62			
19	Peak	61			
'	I Çak	246			
 					
20	Intermediate	59			
21	Intermediate	58			
22	Intermediate	56			
23	Intermediate	52			
	_	225			
24	Night	48			

Weekend Profile	
8 hours/day @ Intermediate Power Level	
16 hours/day @ Night Power Level	

Weekday Totals					
Weekday Totals					
Average Average Weekday					
Period	GW	% Capacity	Hours		
	40.07	00.050/	4.5		
Night	42.67	60.95%	45		
Intermediate	56.36	80.52%	55 22		
Peak	61.50	87.86%	20		
Overall	52.08	74.40%	120		
	•				
	Weeke	nd Totals			
	Average	Average	Weekend		
Period	GW	% Capacity	Hours		
Night	42.67	60.95%	32		
Intermediate	56.36	80.52%	16		
Peak	0.00	0.00%	0		
Overall	47.23	67.47%	48		
	Totals for	Entire Week			
	Average	Average			
Period	GW	% Capacity	Hours		
Night	42.67	60.95%	77		
Intermediate	56.36	80.52%	71		
Peak	61.50	87.86%	20		
Overali	50.70	72.42%	168		

FIG 33
Part Load Efficiency Comparison



		EC	ONOMIC	ECONOMIC COMPARISON	RISON				
Combined	T 5	Fuel	Capital	Main-	Total	Net	Average	XON	Specific
Cycle Plant	Technology	Costs	Costs	tenance Costs	Major Costs	Electricity Produced	Cost Per kWh	Electricity Cost Per Emissions Produced kWh	NOX Emissions
		MM US\$	MM US\$ MM US\$	MM US\$ MM US\$ MM KWh	MM US\$	MM kWh	US\$/ KWh	tons	tons/ MM kWh
General Electric GE S207FA (520 MW)	GE "F" Technology	70.55	22.25	5.78	98.58	3,246	0.0304	35.24	0.0109
725 MW Invention GE "F" Technology Embodiment	GE "F" Technology	91.10	24.01	4.74	119.85	4,512	0.0266	75.99	0.0168
	Net Cost Savings: Annual Savings: \$12.35 20 Year Savings: \$247.08	\$12.35 \$247.08					0.0038		

Westinghouse W 2X1 501G (715 MW)	Westinghouse W "G" Technology W 2X1 501G (715 MW)	93.41	34.11		14.01 141.54 4,453	4,453	0.0318	255.48 0.0574	0.0574
725 MW Invention GE "F" Technology Embodiment	GE "F" Technology	ြ	24.01	.10 24.01 4.74	119.85	4,512 0.0266	0.0266	75.99	0.0168
	Net Cost Savings: Annual Savings: \$23.26 20 Year Savings: \$465.22	: \$23.26 : \$465.22					0.0052		

NOTES: (1) Fuel costs at \$3.00 per MM BTU

(2) Load profile from 60 to 100% utilizing a trend typical for current electrical usage
(3) Capital costs assume a 100% loan at 8% interest for 20 years
(4) Total costs include fuel, capital, and maintenance costs

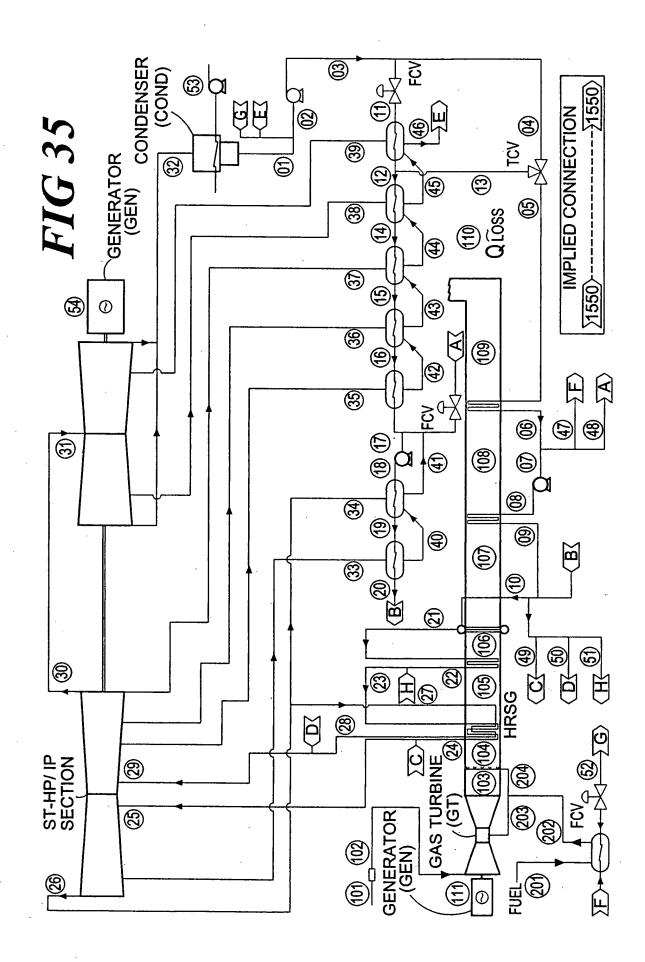


FIG 36

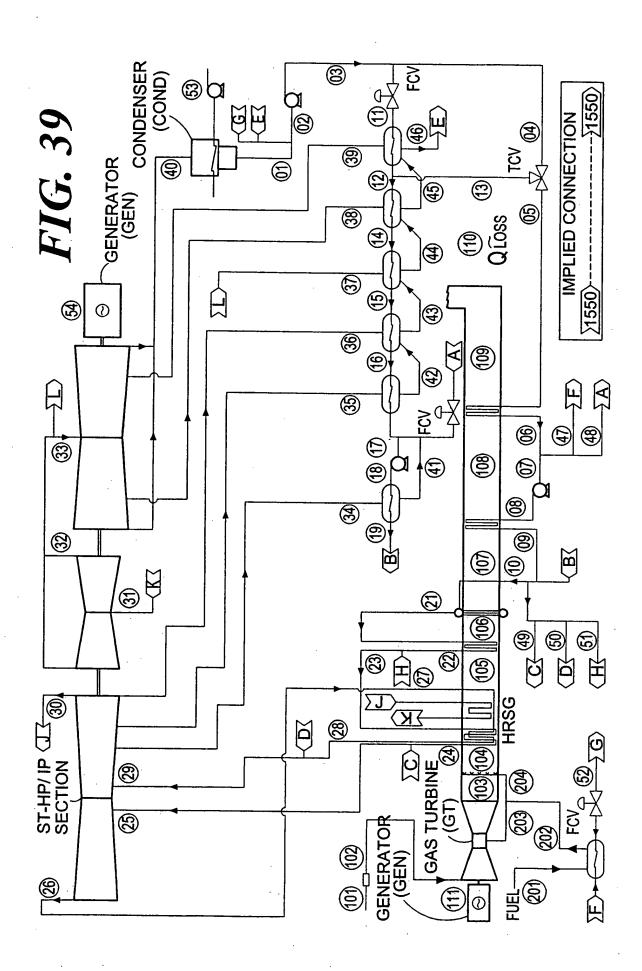
							at Balance
	725 MV	V Combine	ed Cycle wi	th 2 - GE	Frame 7 C	Ts, 2400	psig steam cycle
			Stean	n/Feedw	ater Sys	stem	
Point	Pressure	Temp	Enthalpy	Flow	Heat	Power	Comments
					Input		
	psia	Degrees	BTU/lb	lb/hr	MMBTU	kW	
		F			/hr		
1	0.59			1749377			
2				1956488			
3				1956488		-1169	Pump power, point 2 - 3
4	539.00	86.29	55.793	994750			
5		119.18				ř.	Preheat feedwater to dew point of exhaust gases
6	528.22	386.06	360.471	1775863			
7	528.22	386.06	360.471	1366048			
8						-3676	Pump power, point 7 - 8
9	2913.55	689.56		1366048			
10	2913.55			1776869			
11	550.00	86.29	55.793	961739			
12	539.00	160.93	130.200	180625			
13	550.00	160.93	130.200	781113			Feedwater - Exit FWH 1
14	528.22	229.41	198.872	180625			Feedwater - Exit FWH 2
15	517.66	298.23	268.796	180625			Feedwater - Exit FWH 3
16			327.796	180625			Feedwater - Exit FWH 4
17	497.16	408.59	384.714	180625			Feedwater - Exit FWH 5
18	3002.96	404.80	383.553	599668		-1634	Pump power, point 17 - 18
19	2957.92	496.07	483.061	599668			Feedwater - Exit FWH 6
20	2913.55	561.37	560.245	599668			Feedwater - Exit FWH 7
21	 		1037.440	1776869			Exit Evaporator
22	2684.84	854.67	1336.605	1776869			Exit Superheater Section 1
23	2684.84	845.18	1333.204	1786620			Enter Superheater Section 2
24			1562.578	1786620			Exit Superheater Section 2
25		 	1486.820	1965717			ST HP Section Inlet
26			1327.813	1913817			ST HP Section Outlet
27			1327.813				Enter Reheater Section
28			1544.119	-			Exit Reheater Section
29			1544.119				ST IP Section Inlet
30	64.95		1276.096				ST IP Section Outlet
31	63.65		1276.096				ST LP Section Inlet
32			973.250				ST LP Section Outlet

		Exe	mplary	Prefer	red Em	bodim	ent He	at Balance
		725 MV	V Combine	ed Cycle w	ith 2 - GE	Frame 7 G	Ts, 2400	psig steam cycle
				Stean	n/Feedw	ater Sys	stem	
Poi	nt	Pressure	Temp	Enthalpy		Heat Input	Power	Comments
		psia	Degrees F	BTU/lb	lb/hr	MMBTU /hr	kW	
	33	1100.80	803.31	1386.731	51900			1st Extraction Steam to # 7 Feedwater Heater, 5% Press Drop 2nd Extraction Steam to #
	34	645.12	664.75	1327.813	58489			6 Feedwater Heater, 5% Press Drop 3rd Extraction Steam to # 5
	35	243.32	801.33	1424.375	9462			Feedwater Heater, 5% Press Drop 4th Extraction Steam to # 4
	36	131.39	646.41	1350.853	9411			Feedwater Heater, 5% Press Drop 5th Extraction Steam to # 3
	37	62.36	486.11	1276.096	10580		•	Feedwater Heater, 5% Press Drop
	38	20.94	287.54	1185.142	9914			6th Extraction Steam to # 2 Feedwater Heater, 5% Press Drop
	39	5.45		1094.921	66583			7th Extraction Steam to # 1 Feedwater Heater, 5% Press Drop
L	40	1100.80			51900			
	41	645.12		395.673	110389			
<u> </u>	42	243.32		337.873	9462			
	43	131.39			18873			
	44	62.36			29453			
<u> </u>	45 46	20.94 5.45			39367			
	40	528.22			105951 101161	· ·		
	48				308654			
	49				179097			
	50	2913.55			0			
	51	2913.55		713.255	9750			
	52	528.22			101161			
	53							Pump power, cooling water
								Total Auxiliary Load
	54							ST Generator Output
							383460	Net Steam cycle power

	Exe	mplary	Prefer	red Em	bodim	ent Hea	at Balance
	725 MV	V Combine	ed Cycle w	ith 2 - GE	Frame 7 G	Ts, 2400	psig steam cycle
			G	T/HRSG	System	1	
Point	Pressure	Temp	Enthalpy	Flow	Heat	Power	Comments
					Input		
	psia	Degrees F	BTU/ib	lb/hr	MMBTU /hr	kW	
101	14.70	59.00		6954954			
102	14.59	59.00		6954954			
103	15.18	1123.00	412.64	7103452			
104	15.18	1650.65	573.79	7157276			
105	15.09	1267.65	459.31	7157276			
106	15.00	1002.46	384.29	7157276			
107	14:91	711.24	303.00	7157276			
108	14.82	417.83	223.80	7157276			,
109	14.70	156.55	155.65	7157276			
110					-29.93		HRSG Heat Loss - 1%
111						341540	Net GT power
<u> </u>			F	uel Gas	System	•	
201	500.0	70.00	236.45	202322			_
202	450.0	368.92	385.28	202322			
203	427.5	368.92	385.28	148498	3551.60		
204	45.0	368.92	385.28	53824	1281.87		

-	Totals	4833.47	725000

Heat Rate, HHV	6667
Heat Rate, LHV	6006



	Exe	mplary	Prefer	red En	nbodim	ent He	at Balance
1	1040 MW	Combined	Cycle with	2 - GE Fr	ame 7 GT:	s, Ultrasur	percritical steam cycle
					vater Sy		
Point	Pressure	Temp	Enthalpy	Flow	Heat Input	Power	Comments
	psia	Degrees F	BTU/lb	lb/hr	MMBTU/ hr	kW	
1	0.59	84.66	52.689	2540732			
2	0.59	84.66	53.782	3153031			
3	450.00	86.21	55.450	3153031		-1541	Pump power, point 2 - 3
4	450.00	86.21	55.450	795099			
5		132.71	101.785	1775863			Preheat feedwater to dew point of exhaust gases
6		430.20	408.209	1775863			Exit Economizer 1
7		430.20	408.209	1775863			
8			423.061	1775863		-7728	Pump power, point 7 - 8
9	4044.06	643.52	667.480	1775863			Exit Economizer 2
10	4044.06			3044712			
11	450.00	86.21	55.450	2357932			
12	450.00	170.32	139.348	1377168			Feedwater - Exit FWH 1
13	450.00	170.32	139.348	980764			To TCV
14	450.00	221.51	190.697	1377168			Feedwater - Exit FWH 2
15	450.00	297.81	268.179	1377168			Feedwater - Exit FWH 3
16	450.00	385.80	360.096	1377168			Feedwater - Exit FWH 4
17	427.50	442.21	421.528	1377168			Feedwater - Exit FWH 5
18	4429.20	455.32	439.161	1392731		-6061	Pump power, point 17 - 18
19	4429.20	496.09	483.714	1392731			Feedwater - Exit FWH 6
		<u> </u>		·			
21	4044.06		894.294				Exit Evaporator
22			1078.751				Exit Superheater Section 1
23			1062.496				Enter Superheater Section 2
24			1466.947				Exit Superheater Section 2
25	3851.48		1463.488				ST HP Section Inlet
26			1318.409		·	_	ST HP Section Outlet
27	1049.78		1318.409				Enter Reheater Section 1
28	965.80		1569.531				Exit Reheater Section 1
29	965.80		1569.531				ST IP Section Inlet
30	218.46		1372.625				ST IP Section Outlet
31	200.98		1583.042				ST RH2 Section Inlet
32	72.79	817.36	1439.510	2814556			ST RH2 Section Outlet

	Exe	mplary	/ Prefer	red En	nbodim	ent He	at Balance
1	040 MW (Combined	Cycle with	2 - GE Fr	ame 7 GT:	s, Ultrasu	percritical steam cycle
					vater Sy		
Point	Pressure	Temp	Enthalpy	Flow	Heat	Power	Comments
					Input		
	psia	Degrees	BTU/lb	lb/hr	MMBTU/	kW	
		F			hr		
33	66.97	816.90	1439.510	2740311			ST LP Section Inlet
						-	1st Extraction Steam to # 7
							Feedwater Heater,
34	611.58	986.16	1509.499	50957			5% Press Drop
							2nd Extraction Steam to # 6
م	070.05	0.40.50					Feedwater Heater,
35	370.65	843.53	1441.277	79026			5% Press Drop
							3rd Extraction Steam to # 5
36	200.72	607.00	4272 005	400050			Feedwater Heater,
- 30	209.72	097.02	1372.625	108953			5% Press Drop
							4th Extraction Steam to # 4
37	69.88	817 13	1439.510	74245			Feedwater Heater,
- 0,	05.00	017.13	1433.310	74243			5% Press Drop 5th Extraction Steam to # 3
							Feedwater Heater,
38	19.46	452.21	1303.095	49520			5% Press Drop
			1000.000	40020			6th Extraction Steam to # 2
l				,			Feedwater Heater,
39	6.76	395.80	1207.801	150060			5% Press Drop
40	0.59		1056.410				ST LP Section Outlet
41	611.58		432.802			· · · · · · · · · · · · · · · · · · ·	
42	370.65		370.713				
43	209.72	307.81					
44	69.88	231.51		262224			
45	19.46	180.32		311744			
46	6.76	96.21		461804			
47	427.50		408.227	150496			
48	427.50	430.20		150496			,
49	4044.06			10000			
		607.00		12888			
50	4044.06	607.00		0			
51	4044.06	607.00		110994			***************************************
52	427.50	75.62	44.900	150496			
53							Pump power, cooling water
						-16694	Total Auxiliary Load
54							ST Generator Output
1						698460	Net Steam cycle power

	Exe	mplary	Prefer	red En	nbodim	ent He	at Balance
	040 MW (Combined	Cycle with	2 - GE Fr	ame 7 GTs	s, Ultrasur	percritical steam cycle
			G	T/HRS	3 Systen	n	
Point	Pressure	Temp	Enthalpy	Flow	Heat Input	Power	Comments
	psia	Degrees F	BTU/lb	lb/hr	MMBTU/ hr	kW	
101	14.70	59.00		6910726			
102	14.59	59.00		6910726			
103	15.33	1123.00	412.64	7103452			
104	15.33	2465.24	865.01	7255946			
105	15.20	1363.91	500.48	7255946			
106	15.07	1095.41	422.30	7255946			
107	14.95	689.41	304.60	7255946			
108	14.82	472.67	244.17	7255946			
109	14.70	191.95	168.42	7255946			
110					<i>-</i> 44.73		HRSG Heat Loss - 1%
111						341540	Net GT power

				F	uel Gas	System	
	201	500.0	50.00	227.72	300992		
	202	450.0	411.70	409.38	300992		
-	203	427.5	411.70	409.38	300992	3546.72	
	204	45.0	411.70	409.38	152494	3643.97	

	,	
Totals	7190.69	1040000

Heat Rate, HHV	6914
Heat Rate, LHV	6229

FIG. 43
Exemplary Embodiment Load Transition

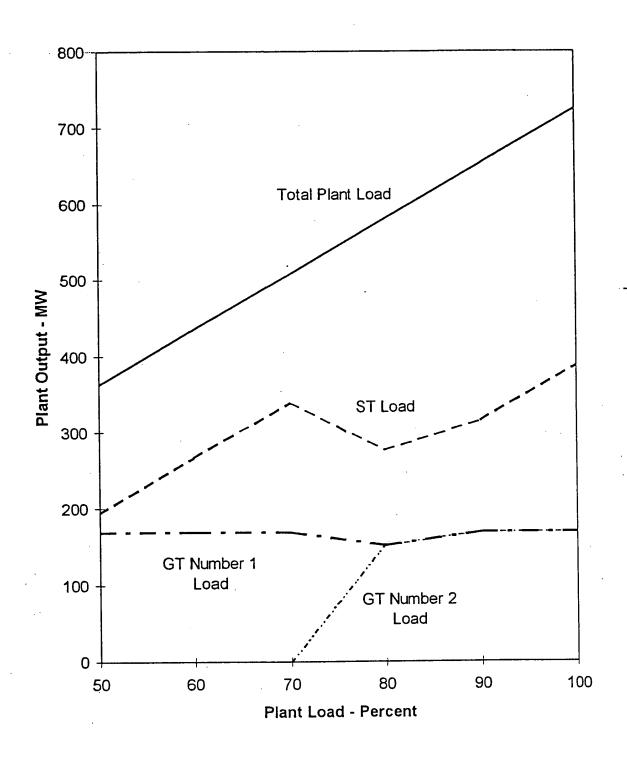
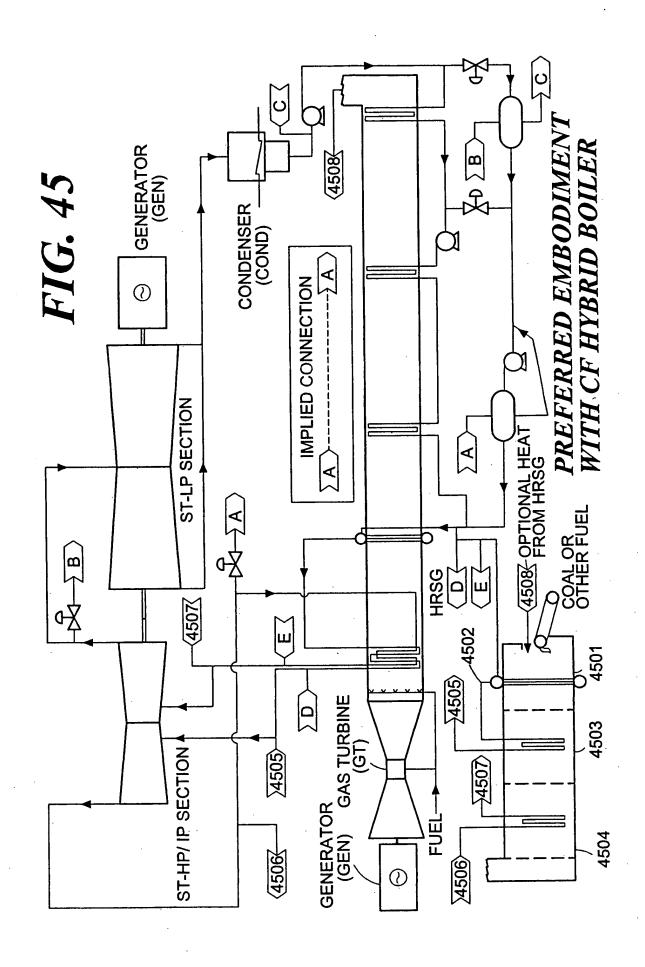


FIG. 44

Retrofit of Existing Steam Plants

Preferred Embodiment vs. Prior Art

			Ste	Steam Turbine	ine								
			Sec	Section Flows	SMC					-			
Technology	Steam	Steam	H	<u>d</u>	م	J.	Gas	Steam	Net	Plant	Cost for	Total	Plant
)	Inlet	Exhaust Section Section Section	Section	Section	Section	Section Turbine	Turbine	Turbine	Plant	Heat	Steam	Plant	Cost
	Press.	Press.	Inlet	Inlet	Inlet	Exhaust Power		Power	Power	Rate	Turbine	Cost	≷
			Flow	Flow	Flow	Flow					Modifi-		
											cations		
	psia	inch	k-lb/hr	k-lb/hr	k-lb/hr	k-lb/hr	MW	MΜ	MW	BTU/	MM	MM	\$/kWh
		HgA								kWh	US\$	US\$	
Conventional Steam	2415	1.20	2,354	2,209	1,815	1,587	0	409	400	7620	N/A	20	125
Plant (pre-retrofit).													
Prior Art - 1 GT	1815	1.20	439	511	528	528	169	97	263	0609	N/A	N/A	N/A
Prior Art - 3 GTs	1815	1.20	1,317	1,533	1,584	1,584	506	299	798	6040	10	240	301
Preferred	2225	1.20	2,182	1,952	1,784	1,593	169	374	535	6235	0	110	206
Embodiment - 1 GT													
Preferred	2100	1.36	2,046	1,946	1,900	1,824	338	394	725	0909	0	170	234
Embodiment - 2 GTs													



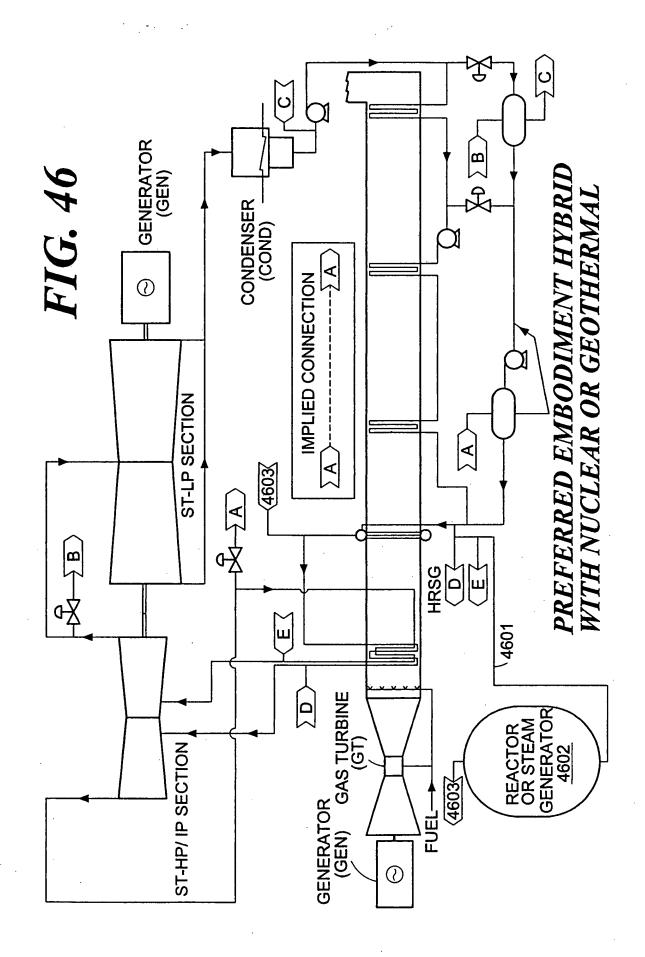


FIG. 47

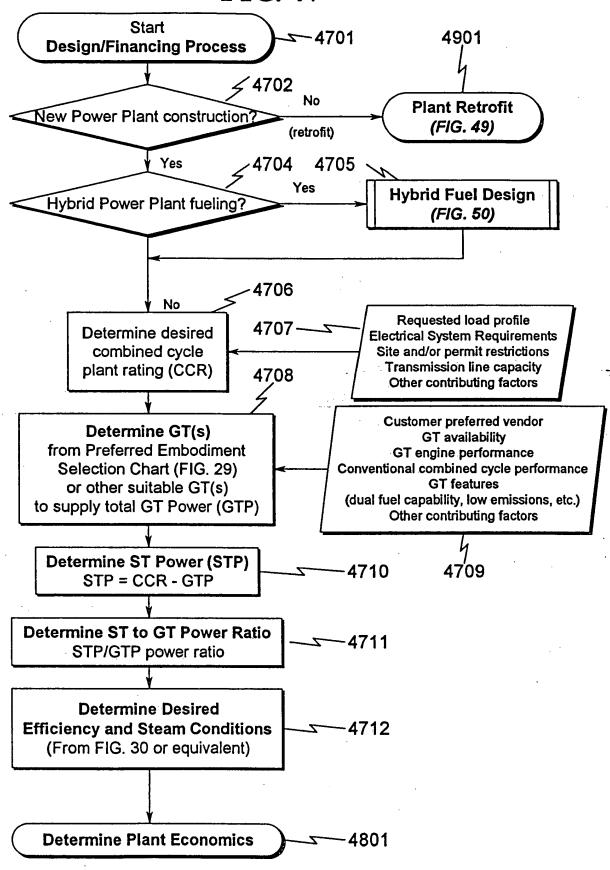


FIG. 48

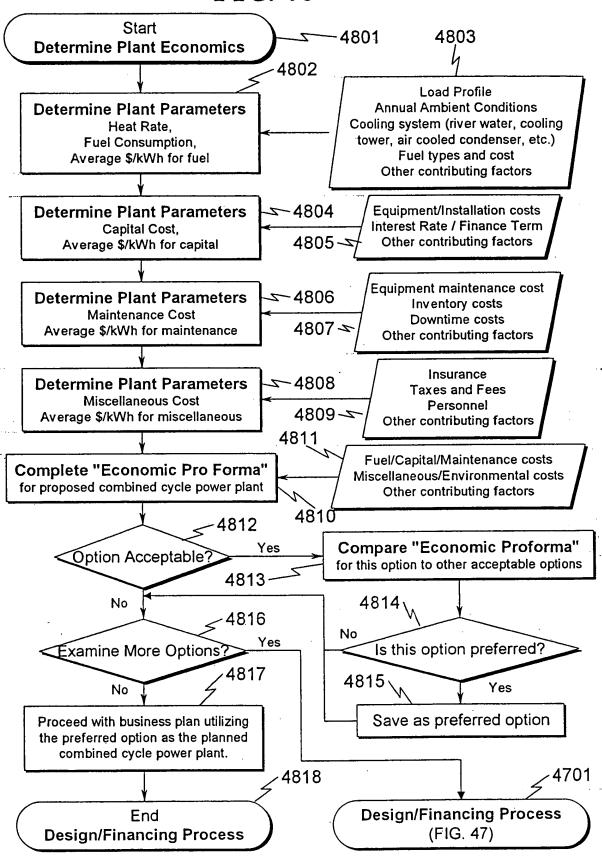


FIG. 49

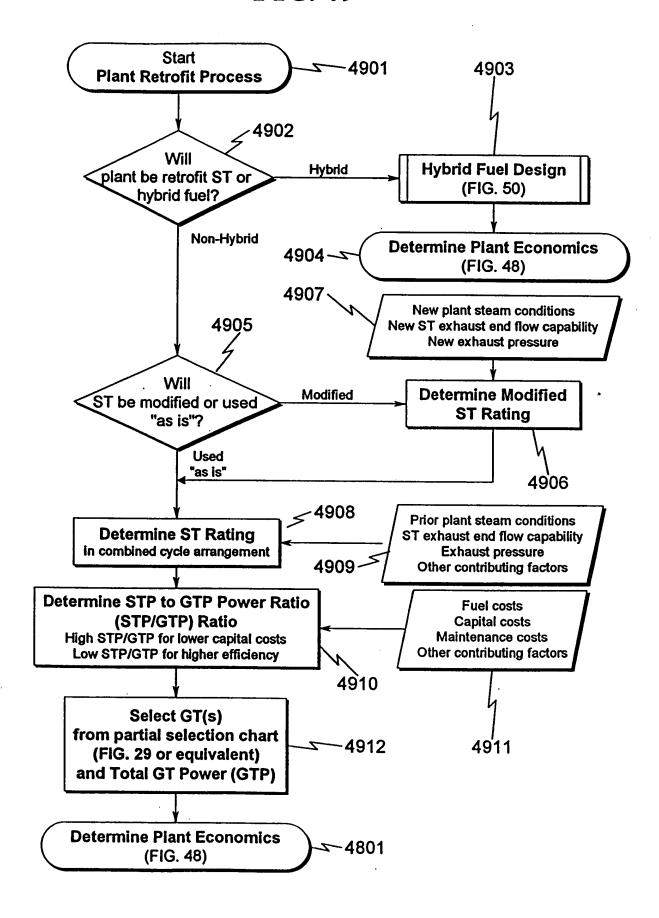


FIG. 50

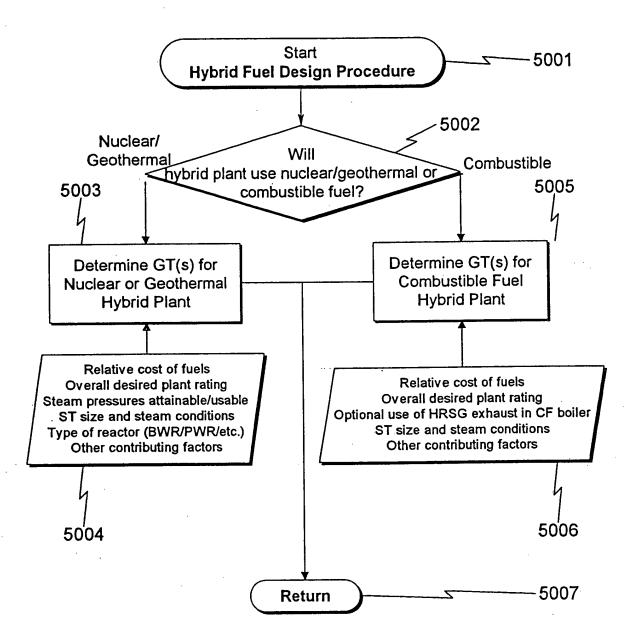
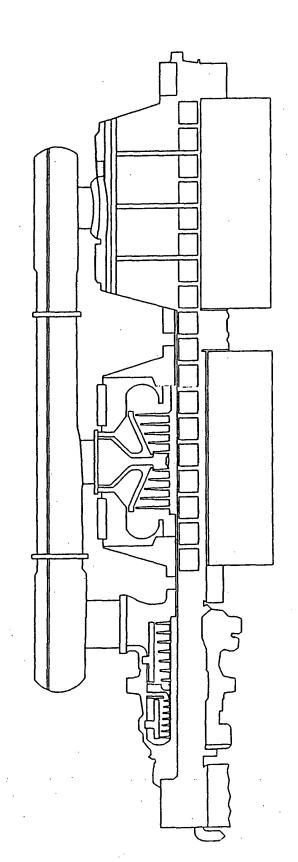


FIG. 51

EXEMPLARY THREE-CASING, FOUR-FLOW STEAM TURBINE (GE)



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